

References

- Adorni, N., Peterlongo, G., Ravetta, R. and Tacconi, F. A., 1964, Large Scale Experiments on Heat Transfer and Hydrodynamics with Steam-water Mixtures, *CISE Report R-91*, Italy.
- Akiyama, M. and Aritomi, M., 2002, *Advanced Numerical Analysis of Two-phase Flow Dynamics—Multi-dimensional Flow Analysis—*, Corona Publishing Co. Ltd., Tokyo, Japan
- Alia, P., Cravarolo, L., Hassid, A. and Pedrocchi, E., 1965, Liquid Volume Fraction in Adiabatic Two-phase Vertical Upflow-round Conduit, *CISE Report-105*, Italy.
- Antal, S. P., Lahey Jr, R. T. and Flaherty, J. E., 1991, Analysis of Phase Distribution in Fully Developed Laminar Bubbly Two-phase Flow, *Int. J. Multiphase Flow* **17**: 635-652.
- Aris, R., 1962, *Vectors, Tensors and the Basic Equations of Fluid Mechanics*, Prentice-Hall, Englewood Cliffs, N.J.
- Arnold, G. S., Drew, D. A. and Lahey Jr., R. T., 1989, Derivation of Constitutive Equations for Interfacial Force and Reynolds Stress for a Suspension of Spheres Using Ensemble Cell Averaging, *Chem. Eng. Comm.* **86**: 43-54.
- Auton, T. R., 1987, The Lift Force on a Spherical Body in a Rotational Flow, *J. Fluid Mech.* **183**: 199-218.
- Azbel, D., 1981, *Two-phase Flows in Chemical Engineering*, Cambridge University Press, Cambridge, UK.
- Azbel, D. and Athanasios, I. L., 1983, A Mechanism of Liquid Entrainment. *Handbook of Fluids in Motion*, Ann Arbor Sci. Pub., Ann Arbor, MI.
- Baker, J. L. L., 1965, Flow-regime Transitions at Elevated Pressure in Vertical Two-phase Flow, *Argonne National Lab. Report*, ANL-7093.
- Bankoff, S. G., 1960, A Variable Density Single-fluid Model for Two-phase Flow with Particular Reference to Steam Water Flow, *J. Heat Transfer* **82**: 265-272.
- Bello, J. K., 1968, *Turbulent Flow in Channel with Parallel Walls*, Moskva, Mir, in Russian.
- Bergonzoli, F. and Halfen, F. J., 1964, Heat Transfer and Void Formation during Forced Circulation Boiling of Organic Coolants, NAA-SR-8906, Atomic International.
- Bilicki, A. and Kestin, J., 1987, Transition Criteria for Two-phase Flow Patterns in Vertical Upward Flow, *Int. J. Multiphase Flow* **13**: 283-294.
- Bird, R. B., Stewart, W. E. and Lightfoot, E. N., 1960, *Transport Phenomena*, John Wiley and Sons, Inc., New York.
- Bornhorst, W. J. and Hatsopoulos, G. N., 1967, Analysis of a Liquid Vapor Phase Change by the Methods of Irreversible Thermodynamics, *J. Applied Mech.* **89**: 847-853.

- Boure, J. and Réocreux, M., 1972, General Equations of Two-phase Flows: Application to Critical Flows and to Non Steady Flows, *4th All Union Heat and Mass Transfer Conference*, Minsk.
- Boure, J., 1973, Dynamique des Écoulements Diphasiques: Propagation des Petites Perturbations, *CEA-R-4456*.
- Bowen, R. M., 1967, Toward a Thermodynamics and Mechanics of Mixtures, *Arch. Rational Mech. Anal.* **24**: 370-403.
- Bridge, A. G., Lapidus, L and Elgin, J. C., 1964, The Mechanics of Vertical Gas-Liquid Fluidized System I: Counter-current Flow, *AIChE J.* **10**: 819-827.
- Brinkman, H., 1952, The Viscosity of Concentrated Suspensions and Solutions, *J. Chem. Phys.* **20**: 571.
- Brodkey, R. S., 1967, *The Phenomena of Fluid Motion*, Addison-Wesley.
- Brodkey, R. S., 1971, Transport Phenomena at the Liquid-Vapor Interface of Mercury Using a Radioactive Tracer, *International Symposium on Two-phase Systems*, Haifa.
- Burgers, J. M., 1941, On the Influence of the Concentration of a Suspension upon the Sedimentation Velocity (in Particular for a Suspension of Spherical Particles) *Proc. K. Ned. Akad. Wet.* **44**: 1045-1051 (1941); **45**: 9-16 (1942)
- Buevich, I., 1969, A Hydrodynamic Model of Disperse Systems, *J. Applied Math. Mech.* **33**: 466-479.
- Buyevich, Y., 1972, Statistical Hydrodynamics of Disperse Systems. Part.I. Physical Background and General Equations, *J. Fluid Mech.* **49**: 489-507.
- Carrier, G. F., 1958, Shock Waves in Dusty Gas, *J. Fluid Mech.* **4**: 376-382.
- Callen, H. B., 1960, *Thermodynamics*, Wiley.
- Chao, B., 1962, Motion of Spherical Gas Bubbles in a Viscous Liquid at Large Reynolds Numbers, *Phys. Fluids* **5**: 69-79.
- Clift, R., Grace, J. R. and Weber, M. E., 1978, *Bubbles, Drops, and Particles*, Academic Press, New York.
- Coleman, B. and Noll, W., 1960, An Approximate Theorem for Functionals with Applications in Continuum Mechanics, *Arch. Rational Mech. Anal.* **6**: 355-370.
- Coleman, B. D., 1964, Thermodynamics of Materials with Memory, *Arch. Rational Mech. Anal.* **17**: 1-46.
- Collier, J., 1972, *Convective Boiling and Condensation*, McGraw Hill, London.
- Coulaloglou, C. A. and Tavlarides, L. L., 1976, Drop Size Distributions and Coalescence Frequencies of Liquid-liquid Dispersion in Flow Vessels, *AIChE J.* **22**: 289-297.
- Coulaloglou, C. A. and Tavlarides, L. L., 1977, Description of Interaction Processes in Agitated Liquid-liquid Dispersions, *Chem. Eng. Sci.* **32**: 1289-1297.
- Cravarolo, L., Giorgini, A., Hassid, A. and Pedrocchi, E., 1964, A Device for the Measurement of Shear Stress on the Wall of a Conduit; Its Application in the Mean Density Determination in Two-phase Flow; Shear Stress Data in Two-phase Adiabatic Vertical Flow, *CISE Report-82*, Italy.
- Culick, F., 1964, Boltzman Equation Applied to a Problem of Two-phase Flow, *Phys. Fluid* **7**: 1898-1904.
- De Groot, S. B. and Mazur, P., 1962, *Non-equilibrium Thermodynamics*, North Holland.
- De Jarlais, G., Ishii and M., Linehan, J., 1986, Hydrodynamic Stability of Inverted Annular Flow in an Adiabatic Simulation, *J. Heat Transfer* **108**: 84-91.
- Delhaye, J. M., 1968, Equations of Fondamentales des Écoulements Diphasiques, Part 1 and 2, *CEA-R-3429*.
- Delhaye, J. M., 1969, General Equations of Two-phase Systems and their Application to Air-water Bubble Flow and to Steam-water Flashing Flow, *ASME Paper 69-HT-63, 11th Heat Transfer Conference*, Minneapolis.

- Delhaye, J. M., 1970, Contribution à L'étude des Écoulements Diphasiques Eau-air et Eau-vapeur, *Ph.D. Thesis*, University of Grenoble.
- Delhaye, J. M., 1974, Jump Conditions and Entropy Sources in Two-phase Systems. Local Instant Formulation, *Int. J. Multiphase Flow* **1**: 395-409.
- Dinh, T. N., Li, G. J. and Theofanous, T. G., 2003, An Investigation of Droplet Breakup in High Mach, Low Weber Number Regime, *Proc. 41st Aerospace Sci. Mtg and Exh.*, Paper AIAA 2003-317, Reno, Nevada.
- Diunin, A. K., 1963, On the Mechanics of Snow Storms, *Siberian Branch, Akademii Nauk SSSR*, Novosibirsk.
- Drew, D. A., 1971, Averaged Field Equations for Two-phase Media, *Studies Appl. Math.* **1**: 133-166.
- Dumitrescu, D. T., 1943, Stomung an einer Luftblase in Senkrechten Rohr, *Z. Angew. Math. Mech.* **23**: 139-149.
- Eilers, H., 1941, The Viscosity of the Emulsion of Highly Viscous Substances as Function of Concentration, *Kolloid Z* **97**: 313-321.
- Ervin, E. A. and Tryggvason, G., 1997, The Rise of Bubbles in a Vertical Shear Flow, *J. Fluids Eng.* **119**: 443-449.
- Fauske, H., 1962, Critical Two-phase, Steam Water Flow, *Proc. Heat Transfer and Fluid Mechanics Institute*, Stanford Univ. Press, pp.78.
- Fick, A., 1855, Über Diffusion, *Ann. Der Phys.* **94**: 59-86.
- Frankl, F. I., 1953, On the Theory of Motion of Sediment Suspensions, *Soviet Physics Doklady, Academii Nauk SSSR*, **92**: 247-250.
- Frankel, N. A. and Acrivos, A., 1967, On the Viscosity of a Concentrated Suspension of Solid Spheres, *Chem. Eng. Sci.* **22**: 847-853.
- Friedlander, S. K., 1977, *Smoke, Dust and Haze*, Wiley, New York.
- Fu, X. Y. and Ishii, M., 2002a, Two-group Interfacial Area Transport in Vertical Air-water Flow I. Mechanistic Model, *Nucl. Eng. Des.* **219**: 143-168.
- Fu, X. Y. and Ishii, M., 2002b, Two-group Interfacial Area Transport in Vertical Air-water Flow II. Model Evaluation, *Nucl. Eng. Des.* **219**: 169-190.
- Goda, H., Hibiki, T. Kim, S., Ishii, M. and Uhle, J., 2003, Drift-flux Model for Downward Two-phase Flow, *Int. J. Heat Mass Transfer* **46**: 4835-4844.
- Gibbs, J. W., 1948, *Collected Work of J. W. Gibbs*, Yale University Press, Vol.1, New York.
- Goldstein, S., 1938, *Modern Developments in Fluid Dynamics*, Oxford University Press, London.
- Govier G. W. and Aziz, K., 1972, *The Flow of Complex Mixtures in Pipes*, Van Nostrand-Reinhold Co., New York.
- Grace, J. R., Wairegi, T. and Brophy, J., 1978, Break-up of Drops and Bubbles in Stagnant Media, *Can. J. Chem. Eng.* **556**: 3-8.
- Hadamard, J., 1911, Mouvement Permanent Lent d'une Sphere Liquide Visqueuse dans un Liquid Visqueux, *C. R. Acad. Sci. Paris Sér A-B* **152**: 1735-1739.
- Hancox, W. T., and Nicoll, W. B., 1972, Prediction of Time-dependent Diabatic Two-phase Water Flows, *Prog. Heat Mass Transfer* **6**: 119-135.
- Happel, J. and Brfnnner, H., 1965, *Low Reynolds Number Hydrodynamics*, Prentice-Hall.
- Harmathy, T. Z., 1960, Velocity of Large Drops and Bubbles in Media of Infinite and Restricted Extent, *AIChE J.* **6**: 281-288.
- Hawksley, P. G. W., 1951, The Effect of Concentration on the Settling of Suspensions and Flow through Porous Media, *Some Aspect of Fluid Flow*, pp.114, Edward Arnold, London.
- Hayes, W. D., 1970, Kinematic Wave Theory, *Proc. Royal Soc. London Ser. A Math. Phys. Sci.* **320**: 209-226.

- Helmholtz, H., 1868, Uber Discontinuirliche Flüssigkeitsbewegungen, *Monatsber. Dtsch. Akad. Wiss. Berlin* pp.215-228.
- Hewitt, G. and Hall Taylor, N. S., 1970, *Annular Two-phase Flow*, Pergamon Press, Oxford.
- Hibiki, T. and Ishii, M., 1999, Experimental Study on Interfacial Area Transport in Bubbly Two-phase Flows, *Int. J. Heat Mass Transfer* **42**: 3019-3035.
- Hibiki, T. and Ishii, M., 2000a, One-group Interfacial Area Transport of Bubbly Flows in Vertical Round Tubes, *Int. J. Heat Mass Transfer* **43**: 2711-2726.
- Hibiki, T. and Ishii, M., 2000b, Two-group Interfacial Area Transport Equations at Bubbly-to-slug Flow Transition, *Nucl. Eng. Des.* **202**: 39-76.
- Hibiki, T., Ishii, M. and Xiao, Z., 2001a, Axial Interfacial Area Transport of Vertical Bubbly Flows, *Int. J. Heat Mass Transfer* **44**: 1869-1888.
- Hibiki, T., Takamasa, T. and Ishii, M., 2001b, Interfacial Area Transport of Bubbly Flow in a Small Diameter Pipe, *J. Nucl. Sci. Technol.* **38**: 614-620.
- Hibiki, T. and Ishii, M., 2002a, Interfacial Area Concentration of Bubbly Flow Systems, *Chem. Eng. Sci.* **57**: 3967-3977.
- Hibiki, T. and Ishii, M., 2002b, Distribution Parameter and Drift Velocity of Drift-flux Model in Bubbly Flow, *Int. J. Heat Mass Transfer* **45**: 707-721.
- Hibiki, T. and Ishii, M., 2002c, Development of One-group Interfacial Area Transport Equation in Bubbly Flow Systems, *Int. J. Heat Mass Transfer* **45**: 2351-2372.
- Hibiki, T. and Ishii, M., 2003a, One-dimensional Drift-flux Model for Two-phase Flow in a Large Diameter Pipe, *Int. J. Heat Mass Transfer* **46**: 1773-1790.
- Hibiki, T. and Ishii, M., 2003b, One-dimensional Drift-flux Model and Constitutive Equations for Relative Motion between Phases in Various Two-phase Flow Regimes, *Int. J. Heat Mass Transfer* **46**: 4935-4948; Erratum, **48**: 1222-1223 (2005).
- Hibiki, T., Situ, R., Mi, Y. and Ishii, M., 2003a, Modeling of Bubble-layer Thickness for Formulation of One-dimensional Interfacial Area Transport Equation in Subcooled Boiling Two-phase Flow, *Int. J. Heat Mass Transfer* **46**: 1409-1423; Erratum, **46**: 3549-3550 (2003).
- Hibiki, T., Situ, R., Mi, Y. and Ishii, M., 2003b, Local Flow Measurements of Vertical Upward Bubbly Flow in an Annulus, *Int. J. Heat Mass Transfer* **46**: 1479-1496.
- Hibiki, T., Takamasa, T. and Ishii, M., 2004, One-dimensional Drift-flux Model and Constitutive Equations for Relative Motion between Phases in Various Two-phase Flow Regimes at Microgravity Conditions, *Proc. 12th Int. Conf. Nucl. Eng.*, Arlington, VA, USA, ICONE12-49037.
- Hirschfelder, J. V., Curtiss, C. F. and Bird, R. B., 1954, *Molecular Theory of Gases and Liquids*, John Wiley and Sons, Inc., New York.
- Hinze, J. W., 1959, *Turbulence*, McGraw-Hill, New York.
- Hughes, T. A., 1958, Steam-water Mixture Density Studies in a Natural Circulation High Pressure System, *Babcock and Wilcox, G. Report* No. 5435.
- Ishii, M. and Zuber, N., 1970, Thermally Induced Flow Instabilities in Two-phase Mixtures, *Proc. 4th International Heat Transfer Conference*, Paris.
- Ishii, M., 1971, Thermally Induced Flow Instabilities in Two-phase Mixture in Thermal Equilibrium, *Ph.D. Thesis*, Georgia Institute of Technology.
- Ishii, M., 1975, Thermo-fluid Dynamic Theory of Two-phase Flow, Collection de la Direction des Etudes et Recherches d'Electricite de France, Eyrolles, Paris, France, 22.
- Ishii, M. and Grolmes, M. A., 1975, Inception Criteria for Droplet Entrainment in Two-phase Concurrent Film Flow, *AIChE J.* **21**: 308-318.
- Ishii, M., Jones, O. C. and Zuber, N., 1975, Thermal Non-equilibrium Effects in Drift Flux Model of Two-phase Flow, *Trans. Am. Nucl. Soc.* **22**: 263-264.

- Ishii, M., 1976, One-dimensional Drift-flux Modeling: One-dimensional Drift Velocity of Dispersed Flow in Confined Channel, *Argonne National Lab. Report*, ANL-76-49.
- Ishii, M., Chawla, T. C. and Zuber, N., 1976, Constitutive Equation for Vapor Drift Velocity in Two-phase Annular Flow, *AIChE J.* **22**: 283-289.
- Ishii, M. and Chawla, T. C., 1979, Local Drag Laws in Dispersed Two-phase Flow, *Argonne National Lab. Report*, ANL-79-105.
- Ishii, M., 1977, One-dimensional Drift-flux Model and Constitutive Equations for Relative Motion between Phases in Various Two-phase Flow Regimes, *Argonne National Lab. Report*, ANL-77-47.
- Ishii, M. and Zuber, N., 1979, Drag Coefficient and Relative Velocity in Bubbly, Droplet or Particulate Flows, *AIChE J.* **25**: 843-855.
- Ishii, M. and Mishima, K., 1981, Study of Two-fluid Model and Interfacial Area, *Argonne National Lab Report* ANL-80-111.
- Ishii, M. and Mishima, K., 1984, Two-fluid Model and Hydrodynamic Constitutive Relations, *Nucl. Eng. Des.* **82**: 107-126.
- Ishii, M. and De Jarlais, G., 1987, Flow Visualization Study of Inverted Annular Flow of Post Dryout Heat Transfer Region, *Nucl. Eng. Des.* **99**: 187-199.
- Ishii, M., Kim, S. and Uhle, J., 2002, Interfacial Area Transport Equation: Model Development and Benchmark Experiments, *Int. J. Heat Mass Transfer* **45**: 3111-3123.
- Ishii, M. and Kim, S., 2004, Development of One-group and Two-group Interfacial Area Transport Equation, *Nucl. Sci. Eng.* **146**: 257-273.
- Kalinin, A. V., 1970, Derivation of Fluid Mechanics Equations for a Two-phase Medium with Phase Changes, *Heat Transfer Soviet Res.* **2**: 83-96.
- Kataoka, I. and Ishii, M. 1987, Drift Flux Model for Large Diameter Pipe and New Correlation for Pool Void Fraction, *Int. J. Heat Mass Transfer* **30**: 1927-1939.
- Kataoka, I. and Serizawa, A., 1995, Modeling and Prediction of Turbulence in Bubbly Two-phase Flow, *Proc. 2nd Int. Conf. Multiphase Flow '95 – Kyoto*, pp. MO2-11-MO2-16.
- Kelly, F. D., 1964, A Reacting Continuum, *Int. J. Engng. Sci.* **2**: 129-153.
- Kelvin, W., 1871, Hydrokinetic Solutions and Observations, *London, Edinburgh and Dublin Philosophical Magazine and Journal of Science Ser.4* **42**: 362-377.
- Kim, W. K. and Lee, K. L., 1987, Coalescence Behavior of two Bubbles in Stagnant Liquids, *J. Chem. Eng. Jpn.* **20**: 449-453.
- Kirkpatrick, R. D. and Lockett, M. J., 1974, The Influence of Approach Velocity on Bubble Coalescence, *Chem. Eng. Sci.* **29**: 2363-2373.
- Kocamustafaogullari, G., 1971, Thermo-fluid Dynamics of Separated Two-phase Flow, *Ph.D. Thesis*, Georgia Institute of Technology.
- Kocamustafaogullari, G., Chen, I. Y. and Ishii, M., 1984, Unified Theory for Predicting Maximum Fluid Particle Size for Drops and Bubbles, *Argonne National Lab. Report*, ANL-84-67.
- Kocamustafaogullari, G. and Ishii, M., 1995, Foundation of the Interfacial Area Transport Equation and its Closure Relations, *Int. J. Heat Mass Transfer* **38**: 481-493.
- Kolev, N., 2002, *Multiphase Flow Dynamics* 1 Fundamentals, 2: Mechanical and Thermal Interactions, Springer-Verlag.
- Kordyban, E., 1977, Some Characteristics of High Waves in Closed Channels Approaching Kelvin-Helmholtz Instability, *J. Fluids Eng.* **99**: 389-346.
- Kotchine, N. E., 1926, Sur la Théorie des Ondes De-choc dans un Fluide, *Bend. Circ. Mat. Palermo* **50**: 305-344.
- Kutateladze, S. S., 1952, Heat Transfer in Condensation and Boiling, *Moscow, AEC-TR-3770*, USAEC Technical Information Service.
- Kynch, G. J., 1952, A Theory of Sedimentation, *Trans. Faraday Soc.* **48**: 166-176.

- Lackme, C., 1973, Two Regimes of a Spray Column in Counter-current Flow, *AIChE Symp. Heat Transfer R. D.* **70**: 59-63.
- Lahey Jr., R. T., Cheng, L. Y., Drew, D. A. and Flaherty, J. E., 1978, The Effect of Virtual Mass on the Numerical Stability of Accelerating Two-phase Flows, *AIChE 71st Annual Meeting*, Miami Beach, Florida.
- Lahey Jr, R. T., Lopez de Bertodano, M. and Jones Jr., O. C., 1993, Phase Distribution in Complex Geometry Conduits, *Nucl. Eng. Des.* **141**: 117-201.
- Lamb, H., 1945, *Hydrodynamics*, Dover, New York.
- Landau, L. D., 1941, Theory of Super Fluidity of Helium II, *Physical Review* **60**: 166-176.
- Landel, R. F., Moser, B. G. and Bauman, A. J., 1965, Rheology of Concentrated Suspensions: Effects of a Surfactant, *Proc. 4th Int. Congress on Rheology*, Brown University, Part 2, pp.663.
- Letan, R. and Kehat, E., 1967, Mechanics of a Spray Column, *AIChE J.* **13**: 443-449.
- Levich, V. G., 1962, *Physicochemical Hydrodynamics*, Prentice-Hall.
- Levy, S., 1960, Steam Slip-theoretical Prediction from Momentum Model, *J. Heat Transfer* **82**: 113-124.
- Lighthill, M. J. and Whitham, G. B., 1955, On the Kinematic Waves I. Flood Movement in Long Rivers, *Proc. Royal Soc. London* **229**: 281-316.
- Liu, T. J., 1993, Bubble Size and Entrance Length Effects on Void Development in a Vertical Channel, *Int. J. Multiphase Flow* **19**: 99-113.
- Loeb, L. B., 1927, *The Kinetic Theory of Gases*, Dover, New York.
- Lopez de Bertodano, M., Lahey Jr., R. T. and Jones, O. C., 1994, Development of a $k-\epsilon$ Model for Bubbly Two-phase Flow, *J. Fluids Eng.* **116**: 128-134.
- Loth, E., Taeibi-Rahni, M. and Tryggvason, G., 1997, Deformable Bubbles in a Free Shear Layer, *Int. J. Multiphase Flow* **23**: 977-1001.
- Lumley, J., 1970, Toward a Turbulent Constitutive Relation, *J. Fluid Mech.* **41**: 413-434.
- Marchaterre, J. F., 1956, The Effect of Pressure on Boiling Density in Multiple Rectangular Channels, *Argonne National Lab. Report*, ANL-5522.
- Martinelli, R. C. and Nelson, D. B., 1948, Prediction of Pressure Drop during Forced Circulation Boiling of Water, *Trans. ASME* **70**: 695-702.
- Maurer, G. W., 1956, A Method of Predicting Steady State Boiling Vapour Fractions in Reactor Coolant Channels, WAPD-BT-19.
- Maxwell, J., 1867, On the Dynamical Theory of Gases, *Phil. Trans. Roy. Soc. London* **157**: 49-88.
- McConnell, A. S., 1957, *Application of Tensor Analysis*, Dover.
- Mei, R. and Klausner, J. F., 1994, Shear Lift Force on Spherical Bubbles, *Int. J. Heat Fluid Flow* **15**: 62-65.
- Meyer, J. E., 1960, Conservation Laws in One-dimensional Hydrodynamics, *Bettis Technical Review* **61**: WAPD-BT-20.
- Miles, J. W., 1957, On the Generation of Surface Waves by Shear Flows, I-IV, *J. Fluid Mech.* **3**: 185-204 (1957); **6**: 568-582 (1959); **6**: 583-598 (1959); **13**: 433-448 (1962).
- Mishima, K. and Ishii, M., 1980, Theoretical Prediction of Onset of Slug Flow, *J. Fluid Eng.* **102**: 441-445.
- Mishima, K. and Ishii, M., 1984, Flow Regime Transition Criteria for Upward Two-phase Flow in Vertical Tubes, *Int. J. Heat Mass Transfer* **27**: 723-737.
- Miller, J. W., 1993, An Experimental Analysis of Large Spherical Cap Bubbles Rising in an Extended Liquid, *M. S. Thesis*, Purdue University.
- Mokeyev, Yu. G., 1977, Effect of Particle Concentration on their Drag and Induced Mass, *Fluid Mech.-Soviet Res.* **6**: 161-168.

- Muller, I., 1968, A Thermodynamics Theory of Mixtures of Fluids, *Arch. Rational Mech. Anal.* **28**: 1-39.
- Murray, S. O., 1954, On the Mathematics of Fluidization I, Fundamental Equations and Wave Propagation, *J. Fluid Mech.* **21**: 465-493.
- Neal, L. G., 1963, An Analysis of Slip in Gas-liquid Flow Applicable to the Bubble and Slug Flow Regimes, *Kjeller Research Establishment Report, Norway KR-2*.
- Nicklin, D. J., Wilkes, J. O. and Davidson, J. F., 1962, Two-phase Flow in Vertical Tubes, *Trans. Inst. Chem. Eng.* **40**: 61-68.
- Nikuradse, J., 1932, Gesetzmäßigkeit der Turbulenten Strömung in Glatten Rohre, *Forsch. Arb. Ing.-Wes.* pp.356.
- Oolman, T. O. and Blanch, H. W., 1986a, Bubble Coalescence in Air-Sparged Bioreactors, *Biotech. Bioeng.* **28**: 578-584.
- Oolman, T. O. and Blanch, H. W., 1986b, Bubble Coalescence in Stagnant Liquids, *Chem. Eng. Commun.* **43**: 237-261.
- Otake, T., Tone, S., Nakao, K., and Mitsuhashi, Y., 1977, Coalescence and Breakup of Bubbles in Liquids, *Chem. Eng. Sci.* **32**: 377-383.
- Pai, S. I., 1962, *Magnetogasdynamics and Plasma Dynamics*, Wien Springer-Verlag.
- Pai, S. I., 1971, Fundamental Equations of a Mixture of Gas and Small Spherical Solid Particles from Simple Kinetic Theory, *Int. Sym. on Two-phase Systems*, Paper 6-6, Haifa, Israel.
- Pai, S. I., 1972, A New Classification of Two-phase Flows, *J. Mach. Phys. Sci.* **6**: 137-161.
- Panton, R., 1968, Flow Properties for the Continuum View-point of a Non-Equilibrium Gas-Particle Mixture, *J. Fluid Mech.* **31**: 273-303.
- Peebles, F. N. and Garber, H. J., 1953, Studies on the Motion of Gas Bubbles in Liquid, *Chem. Eng. Prog.* **49**: 88-97.
- Petrick, M., 1962, A Study of Vapor Carryunder and Associated Problems, *Argonne National Lab. Report, ANL-65-81*.
- Phillips, M. C. and Riddiford, A. C., 1972, Dynamic Contact Angles 2. Velocity and Relaxation Effects for Various Liquids, *J. Colloid Interface Sci.* **41**: 77-85.
- Pierre, C. C. St., 1965, Frequency-response Analysis of Steam Voids to Sinusoidal Power Modulation in a Thin-walled Boiling Water Coolant Channel, *Argonne National Lab. Report, ANL-7041*.
- Prigogine, I. and Mazur, P., 1951, On Two-phase Hydrodynamic Formulations and the Problem of Liquid Helium II, *Physica* **17**: 661-679.
- Prince, M. J. and Blanch, H. W., 1990, Bubble Coalescence and Break-up in Air-Sparged Bubble Columns, *AIChE J.* **36**: 1485-1497.
- Prosperetti, A., 1999, Some Considerations on the Modeling of Disperse Multiphase Flows by Averaged Equations, *JSME Intl. J., Ser. B*, **42**: 573-585.
- Réocreux, M., Barriere, G. and Vernay, B., 1973, Etude Expérimentale des Débits Critiques en Écoulement Diphasique Eau-vapeur à Faible Titre sur un Canal à Divergent de 7 Degrés, *Cen. G, Rapport* TT 115.
- Réocreux, M., 1974, Contribution à l'étude des Débits Critiques en Élement Diphasique eau Vapeur, *Ph. D. Thesis*, University of Grenoble.
- Richardson, J. F. and Zaki, W. N., 1954, Sedimentation and Fluidization: Part 1, *Trans. Inst. Chem. Eng.* **32**: 35-53.
- Roscoe, R., 1952, The Viscosity of Suspensions of Rigid Spheres, *Br. J. Appl. Phys.* **3**: 267-269.
- Rose, S. C. and Griffith, P., 1965, Flow Properties of Bubbly Mixtures, *ASME Paper* 65-HT-8.
- Rotta, J. C., 1972, *Turbulence Stromungen*, B. G. Teubner, Stuttgart, Germany.

- Rouhani, S. Z. and Becker, K. M., 1963, Measurement of Void Fractions for Flow of Boiling Heavy Water in a Vertical Round Duct, AE-106, Aktiebolaget Atomenergi, Sweden.
- Rybczynski, W., 1911, Über die Fortschreitende Bewegung einer Flüssigen Kugel in einem Zähnen Medium, *Bull. Int. Acad. Sci. Cracov.* **1911A**: 40-46.
- Saffman, P. G., 1965, The Lift on a Small Sphere in a Slow Shear Flow, *J. Fluid Mech.* **22**: 385-400.
- Sato, Y., Sadatomi, M. and Sekoguchi, K., 1981, Momentum and Heat Transfer in Two-phase Bubble Flow - 1. Theory, *Int. J. Multiphase Flow* **7**: 167-177.
- Schlichting, H., 1979, *Boundary Layer Theory*, McGraw-Hill Book Co.
- Schwartz, K., 1954, Investigation of Distribution of Density, Water and Steam Velocity and of the Pressure Drop in Vertical Horizontal Tubes, *VDI Forschungsh.* **20**, Series B, 445.
- Schwartz, A. M. and Tejada, S. B., 1972, Studies of Dynamic Contact Angles on Solids, *J. Colloid Interface Sci.* **38**: 359-375.
- Scriven, L. E., 1960, Dynamics of Fluid Interface, Equation of Motion for Newtonian Surface Fluids, *Chem. Eng. Sci.* **2**: 98-108.
- Serizawa, A., Kataoka, I. and Michiyoshi, I., 1975, Turbulence Structure of Air-water Bubbly Flow, I, II and III, *Int. J. Multiphase Flow* **2**: 221-259.
- Serizawa, A. and Kataoka, I., 1988, Phase Distribution in Two-phase Flow, *Transient Phenomena in Multiphase Flow*, Hemisphere, Washington DC, pp.179-224.
- Serizawa, A. and Kataoka, I., 1994, Dispersed Flow-I., *Multiphase Science and Technology*, Vol. 8, Begell House Inc., New York, pp.125-194.
- Serrin, J., 1959, *Handbuch der Physik*, Vol.8/I, Springer-Verlag.
- Sevik, M. and Park, S. H., 1973, The Splitting of Drops and Bubbles by Turbulent Fluid Flow, *J. Fluids Eng.* **95**: 53-60.
- Slattery, J. C., 1964, Surface - I. Momentum and Moment-of-momentum Balance for Moving Surfaces, *Chem. Eng. Sci.* **19**: 379-385.
- Slattery, J. C., 1972, *Momentum, Energy and Mass Transfer in Continua*, McGraw-Hill Book Co.
- Smissaert, G. E., 1963, Two-component Two-phase Flow Parameters for Low Circulation Rages, *Argonne National Lab. Report*, ANL-67-55.
- Soo, S. L., 1967, *Fluid Dynamics of Multiphase Systems*, Ginn Blaisdell.
- Sridhar, G. and Katz, J., 1995, Drag and Lift Forces on Microscopic Bubbles Entrained by a Vortex, *Phys. Fluids* **7**: 389-399.
- Standart, G., 1964, The Mass, Momentum and Energy Equations for Heterogeneous Flow Systems, *Chem. Eng. Sci.* **19**: 227-236.
- Standart, G., 1968, The Second Law of Thermodynamics for Heterogeneous Flow Systems III. Effect of Conditions of Mechanical Equilibrium and Electroneutrality on Simultaneous Heat and Mass Transfer and Prigogine Theorem, *Chem. Eng. Sci.* **23**: 279-285.
- Stefan, J., 1871, Über das Gleichgewicht und die Bewegung, Insbesondere die Diffusion von Gasmengen, *Sitzgsber, Akad. Wiss. Wien* **63**: 63-124.
- Stewart, C. W., 1995, Bubble Interaction in Low-viscosity Liquids, *Int. J. Multiphase Flow* **21**: 1037-1046.
- Stokes, G. G., 1851, On the Effect of Internal Friction of Fluids on the Motion of Pendulums, *Trans. Cambr. Phil. Soc.* **9**, Part II: 8-106 or Coll. Papers III: 55.
- St. Pierre, C. C., 1965, Frequency-response Analysis of Steam Voids to Sinusoidal Power Modulation in a Thin-walled Boiling Water Coolant Channel, *Argonne National Lab. Report*, ANL-7041.
- Sun, X., Ishii, M. and Kelly, J. M., 2003, Modified Two-fluid Model for the Two-group Interfacial Area Transport Equation, *Annals Nucl. Energy* **30**: 1601-1622.

- Sun, X., Kim, S., Ishii, M. and Beus, S. G., 2004a, Modeling of Bubble Coalescence and Disintegration in Confined Upward Two-phase Flow, *Nucl. Eng. Des.* **230**: 3-26.
- Sun, X., Kim, S., Ishii, M. and Beus, S. G., 2004b, Model Evaluation of Two-group Interfacial Area Transport Equation for Confined Upward Flow, *Nucl. Eng. Des.* **230**: 27-47.
- Taylor, G. I., 1932, The Viscosity of a Fluid Containing Small Drops of Another Fluid, *Proc. R. Soc.* **A138**: 41-48.
- Taylor, G. I., 1934, The Formation of Emulsions in Definable Fields of Flow, *Proc. Royal Soc. London* **A146**: 501-523.
- Teletov, S. G., 1945, Fluid Dynamic Equations for Two-phase Fluids, *Soviet Physics Doklady, Akademii Nauk SSSR* **50**: 99-102.
- Teletov, S. G., 1957, On the Problem of Fluid Dynamics of Two-phase Mixtures, I. Hydrodynamic and Energy Equations, *Bull. the Moscow University* **2**: 15.
- Theofanous, T. G., Li, G. J. and Dinh, T. N., 2004, Aerobreakup in Rarefied Supersonic Gas Flows, *J. Fluid Eng.* **126**: 516-527.
- Thomas, D. G., 1965, Transport Characteristics of Suspension: VIII A Note on Viscosity of Newtonian Suspensions of Uniform Spherical Particles, *J. Colloid Sci.* **20**: 267-277.
- Thome, R. J., 1964, Effect of a Transverse Magnetic Field and Vertical Two-phase Flow through a Rectangular Channel, *Argonne National Lab. Report*, ANL-6854.
- Tomiyama, A., Zun, I., Sou, A. and Sakaguchi, T., 1993, Numerical Analysis of Bubble Motion with the VOF method, *Nucl. Eng. Des.* **141**: 69-82.
- Tomiyama, A., Sou, A., Zun, I., Kanami, N. and Sakaguchi, T., 1995, Effects of Eötvös Number and Dimensionless Liquid Volumetric Flux on Lateral Motion of a Bubble in a Laminar Duct Flow, *Advances in Multiphase Flow*, Elsevier, pp.3-15.
- Tomiyama, A., Tamai, H., Zun, I. and Hosokawa, S., 2002, Transverse Migration of Single Bubbles in Simple Shear Flows, *Chem. Eng. Sci.* **57**: 1849-1858.
- Tong, L. S., 1965, *Boiling Heat Transfer and Two-phase Flow*, John Wiley and Sons, Inc., New York.
- Truesdell, C. and Toupin, R., 1960, The Classical Field Theories, *Handbuch der Physik*, Vol.3/I, Springer-Verlag.
- Truesdell, C., 1969, *Rational Thermodynamics*, McGraw-Hill Book Co.
- Tsouris, C. and Tavlarides, L. L., 1994, Breakage and Coalescence Models for Drops in Turbulent Dispersions, *AIChE J.* **40**: 395-406.
- Tsuchiya, K., Miyahara, T. and Fan, L. S., 1989, Visualization of Bubble-wake Interactions for a Stream of Bubbles in a Two-dimensional Liquid-solid Fluidized Bed, *Int. J. Multiphase Flow* **15**: 35-49.
- Vernier, P. and Delhay, J. M., 1968, General Two-phase Flow Equations Applied to the Thermohydrodynamics of Boiling Nuclear Reactors, *Energie Primaire* **4**: No.1.
- Von Karman, 1950, Unpublished Lectures (1950-1951) at Sorbonne and Published by Nachbar et al. in *Quart. Appl. Math.* **7**: 43 (1959).
- Wallis, G. B., Steen, D. A., Brenner, S. N. and Turner T. M., 1964, Joint U. S. – Euratom Research and Development Program, *Quarterly Progress Report*, January, Dartmouth College.
- Wallis, G. B., 1969, *One-dimensional Two-phase Flow*, McGraw-Hill Book Co.
- Wallis, G. B., 1974, The Terminal Speed of Single Drops or Bubbles in an Infinite Medium, *Int. J. Multiphase Flow* **1**: 491-511.
- Wang, S. K., Lee, S. J., Jones Jr., O. C. and Lahey Jr. R. T., 1987, 3-D Turbulence Structure and Phase Distribution Measurements in Bubbly Two-phase Flows, *Int. J. Heat Mass Transfer* **13**: 327-343.

- Weatherburn, C. E., 1927, *Differential Geometry of Three Dimensions*, Cambridge University Press.
- Werther, J., 1974, Influence of the Bed Diameter on the Hydrodynamics of Gas Fluidized Beds, *AIChE Symp. Ser.* No. 141 70: 53.
- Whitaker, S., 1968, *Introduction to Fluid Mechanics*, Prentice-Hall, Inc.
- White, E. T. and Beardmore, R. H., 1962, The Velocity of Rise of Single Cylindrical Air Bubbles through Liquid Contained in Vertical Tubes, *Chem. Eng. Sci.* **17**: 351-361.
- Wu, Q. and Ishii, M., 1996, Interfacial Wave Instability of Co-current Two-phase Flow in Horizontal Channel, *Int. J. Heat Mass Transfer* **39**: 2067-2075.
- Wu, Q., Kim, S., Ishii, M. and Beus, S. G., 1998, One-group Interfacial Area Transport in Vertical Bubbly Flow, *Int. J. Heat Mass Transfer* **41**: 1103-1112.
- Wundt, H., 1967, Basic Relationships in n-components Diabatic Flow, *EUR* 3459e.
- Yoshida, F. and Akita, K., 1965, Performance of Gas Bubble Columns: Volumetric Liquid-phase Mass Transfer Coefficient and Gas Holdup, *AIChE J.* **11**: 9-13.
- Zhang, D. Z., 1993, Ensemble Phase Averaged Equations for Multiphase Flows, *Ph.D. Thesis*, Johns Hopkins University.
- Zhang, D. Z., Prosperetti, A., 1994a, Averaged Equations for Inviscid Disperse Two-phase Flow, *J. Fluid Mech.* **267**: 185-219.
- Zhang, D. Z., Prosperetti, A., 1994b, Ensemble Phase-averaged Equations for Bubbly Flows, *Phys. Fluids* **6**: 2956-2970.
- Zuber, N., 1964a, On the Dispersed Flow in the Laminar Flow Regime, *Chem. Eng. Sci.* **19**: 897-917.
- Zuber, N., 1964b, On the Problem of Hydrodynamic Diffusion in Two-phase Flow Media, *Proc. 2nd All Union Conference on Heat and Mass Transfer*, Minsk, USSR, **3**: 351.
- Zuber, N., Staub, F. W. and Bijwaard, G., 1964, Steady state and Transient Void Fraction in Two-phase Flow Systems, Vol.1, *GEAP* 5417.
- Zuber, N. and Findlay, J. A., 1965, Average Volumetric Concentration in Two-phase Flow Systems, *J. Heat Transfer* **87**: 453-468.
- Zuber, N. and Staub, F. W., 1966, Propagation and the Wave Form of the Volumetric Concentration in Boiling Water Forced Convection Systems under Oscillatory Conditions, *Int. J. Heat Mass Transfer* **9**: 871-895.
- Zuber, N., 1967, Flow Excursions and Oscillations in Boiling, Two-phase Flow Systems with Heat Addition, *Proc. Symp. Two-phase Flow Dynamics*, **1**: 1071.
- Zuber, N. and Dougherty, D. E., 1967, Liquid Metals Challenge to the Traditional Methods in Two-phase Flow Investigations, *Proc. EURATOM Symposium on Two-phase Flow Dynamics*, pp.1085.
- Zuber, N., Staub, F. W., Bijwaard, G. and Kroeger, P. G., 1967, Steady State and Transient Void Fraction in Two-phase Flow Systems, *General Electric Co. Report GEAP-5417*, vol.1
- Zuber, N., 1971, Personal Communication at Georgia Institute of Technology.
- Zun, I., 1988, Transition from Wall Void Peaking to Core Void Peaking in Turbulent Bubbly Flow, *Transient Phenomena in Multiphase Flow*, Hemisphere, Washington DC, pp.225-245.

Nomenclature

Latin

A	surface of a volume
A	frontal area of bubble
$A^{\alpha\beta}$	surface metric tensor (Aris, 1962)
\mathcal{A}	turbulence anisotropy tensor
A_d	projected area of a typical particle
A_i	mathematical surface between A_1 and A_2
A_i	surface area
A_k	surface bounding the interfacial region and adjacent to phase k
A_m	surface of fixed mass volume
A_p	projected area of a particle
a	cross sectional radius of cap or slug bubble
a_c^i	mobility of the fluid at the interface
a_i	interfacial area concentration
a_{sk}, a_{tk}	isentropic and isothermal sound velocities based on the average thermodynamic properties
B_d	volume of a typical particle
B_S	balance at an interface
B_V	balance in each phase
b_k^F, b_k^M, b_k^E	Transport coefficients associated with interfacial

	transfer of mass, momentum and energy
C	wave velocity
C	constant
C_D	drag coefficient
$C_{D\infty}$	ideal drag coefficient
C_g	variable defined by $\sqrt{2g\Delta\rho/\rho_f}$
C_{hk}	distribution parameter
C_{hm}	mixture-enthalpy-distribution parameter
C_i	closed curve on an interface
C_K	kinematic wave velocity
C_{LW}	coefficient of lift force caused by slanted wake
C_M	virtual mass constant
C_T	adjustable parameter
C_{vk}	distribution parameter
C_{vm}	virtual volume coefficient
C_{vm}	mixture-momentum-distribution parameter
C_τ	distribution parameter
$C_{\psi k}$	distribution parameter for flux
C^i	shape factor
C_0	distribution parameter
C_∞	propagation velocity
C_∞	asymptotic value of distribution parameter
c_k	mass concentration of phase k
c_{pk}, c_{vk}	specific heat at constant pressure and density based on averaged properties
D	hydraulic-equivalent diameter
D^*	length scale ratio
D_b	bubble diameter
D_{bc}	critical bubble size
D_{cl}^*	ratio of D_{crit} to D_{Sm1}
$D_{c,max}$	maximum diameter of stable bubble
D_{crit}	volume-equivalent diameter of a bubble at boundary between groups 1 and 2
$D_{d,max}$	maximum distorted bubble limit

D_d^*	ratio of bubble diameter to bubble diameter at distorted bubble limit
D_e	volume-equivalent diameter of a fluid particle
D_e	eddy diameter
D_E	effective diameter of mixture volume that contains one bubble
D_H	hydraulic-equivalent diameter
D_H^*	non-dimensional hydraulic-equivalent diameter
D_k	diffusion coefficient
D_k	total deformation tensor of phase k
D_{kb}	bulk deformation tensor
D_{ki}	interfacial extra deformation tensor
D_k^α	drift coefficient
D_{Sm}	Sauter mean diameter
D_s	surface-equivalent diameter of a fluid particle
d_B	bubble diameter
\widehat{d}_B	cross-sectional mean diameter of bubbles
E_B	average energy required for bubble breakup
E_d	area fraction of liquid entrained in gas core from total liquid area at any cross section
E_e	average energy of a single eddy
E_k	total energy gain through interfaces for phase k
E_m	mixture total energy source from interfaces
E_m^H	mixture energy gain due to changes in mean curvature
E_o	Eötvös number
$\widehat{e}_k, \widehat{e}_{ki}$	weighted mean virtual internal energy (with turbulent kinetic energy included) at the bulk phase and at the interfaces
$F(\mathbf{x}, t)$	general function
\mathbf{F}^B	Basset force
\mathbf{F}^D	standard drag force
\mathbf{F}^L	lift force
\mathbf{F}^T	turbulent dispersion force
\mathbf{F}^V	virtual mass force

F^W	wall lift force
F_D	drag force
F_k, \mathcal{F}_k	general function associated with phase k
$f(\mathbf{x}, t)$	function for interface position
$f(\mathbf{x}, t, \boldsymbol{\xi})$	molecular density function
f	collision frequency
f	friction factor
f^*	correction factor for drag coefficient
f_i	interfacial friction factor
f_k	Helmholtz potential
$f_{kn}(\mathbf{x}, t, \boldsymbol{\xi})$	particle density function of the n^{th} -kind particles
f_{TW}	two-phase friction factor
G	mass velocity
G	cap bubble thickness
G_s	non-dimensional velocity gradient
g	gravity field
g_k	body force field
$g_k, \widehat{g}_k, \widehat{g}_{ki}$	Gibbs free energy: local instant, bulk mean and interfacial mean values
g_{ln}	space metric tensor (Aris, 1962)
g_N	normal gravitational acceleration
$H_{21}, \overline{\overline{H}}_{21}$	local instant and averaged mean curvature ($\overline{\overline{H}}_{21} > 0$ if phase 2 is the dispersed phase)
h	bubble height
h_1, h_2	average thickness of upper (1) and lower (2) fluid layers
$\widehat{h}_k, \widehat{h}_{ki}$	weighted mean virtual enthalpy (with turbulent kinetic energy included) at the bulk phase and at the interfaces
h_m	mixture virtual enthalpy
I	unit tensor
I_k	interfacial source term in the balance equations for phase k
I_m	interfacial source term for mixture balance equations
I_{ka}, I_{ma}	interfacial source terms in the shock conditions for

	phase k and for mixture
\hat{i}_k, \hat{i}_k	local instant and mean enthalpies
\hat{i}_{ki}	mean enthalpy of phase k at interfaces
\hat{i}_m	mixture enthalpy
i_a	local instant surface enthalpy per area
J	flux
J^D	drift flux
J_a	line flux for interface
J_k	surface flux for phase k
J_k^T, J^T	turbulent fluxes
J_k, J_m	Jacobians based on macroscopic field
\hat{j}_k, \hat{j}	volumetric fluxes of phase k and mixture
j^*	non-dimensional mixture volumetric flux
j^+	non-dimensional mixture volumetric flux
K	constant
K_k	thermal conductivity
\mathbb{K}_k	thermal conductivity tensor
K_k^T	turbulent conductivity
K_k^{T*}	thermal mixing length coefficient
k	wave number
k^{SI}	turbulent kinetic energy due to shear-induced turbulence
k_e	wave number of eddy
L	pitch of slug unit
L_b	cylindrical bubble length
$1/L_j$	area concentration of j^{th} -interface
$1/L_s$	total area concentration
L_T	mean traveling distance between two bubbles for one collision
L_W	effective wake length
l	mixing length
l_B	mixing length due to bubble-induced turbulence
l_{SP}	mixing length of single-phase flow
l_{TP}	mixing length of two-phase flow
m_e	mass per a single eddy

$\dot{m}_k, \overline{\dot{m}_k}$	local instant and mean mass transfer rates per unit area (mass loss)
M	Morton number
M_F	frictional pressure gradient in multi-particle system
$M_{F\infty}$	frictional pressure gradient in single particle system
M_{ik}	generalized interfacial drag
M_k, M_s	state density functions for phase k and interface
M_k, M_m	momentum sources for phase k and mixture
M_m^H	force due to changes in mean curvature
M_k^n, M_k^t, M_k^d	form, skin and total drag forces
$M_{\tau m}$	force associated with mixture transverse stress gradient
\mathbf{N}	unit normal vector to a curve on an interface
N	number of samples
N_b	number of bubbles
N_D	drift number
N_{drag}	drag number
N_e	number of eddies of wave number k_e per volume of fluid
N_{Ec}	Eckert number
N_{Eu}	Euler number
N_{Fr}	Froude number
N_i	converted enthalpy ratio
N_{Jk}	Jakob number
N_{pch}	phase change number
N_{pch}^i	interfacial phase change effect number
N_{Pe}	Peclet number
N_{Prk}^T	turbulent Prandtl number
N_q	interface heating number
N_{Re}	Reynolds number
N_{Re}^i	interfacial Reynolds number
N_{Sl}	Strouhal number
N_{We}	Weber number
N_σ	surface tension number

N_{Pr}	Prandtl number
N_W	number of bubbles inside effective volume
N_μ	viscosity number
N_ρ	density ratio
n	fluid particle number per unit mixture volume
\mathbf{n}	unit normal vector
n_b	bubble number density
n_e	number of eddies of wave number per volume of two-phase mixture
\mathbf{n}_k	outward unit normal vector for phase k
P^{SI}	production of shear-induced turbulence
P_C	probability for a bubble to move toward neighboring bubble
\overline{P}_k	partial pressure tensor
P_i	interfacial wetted perimeter
P_{wf}	wall wetted perimeter
p	pressure
p_c	critical pressure
$p_k, \overline{\overline{p}}_k, \overline{\overline{p}}_{ki}$	partial, bulk mean and interfacial mean pressure
p_m	mixture pressure
\mathbf{q}	heat flux
\mathbf{q}^D	diffusion (drift) heat flux
$\overline{\overline{\mathbf{q}}}_k, \overline{\overline{\mathbf{q}}}_k^T$	mean conduction and turbulent heat fluxes
$\overline{\overline{\mathbf{q}}}, \overline{\overline{\mathbf{q}}}^T$	mixture conduction and turbulent heat fluxes
\dot{q}_k	local instant body heating
$\overline{\overline{q}}_k''$	average heat transfer per interfacial area (energy gain)
\mathbf{q}_k^C	mean conduction heat flux
R	ideal gas constant
R	radius of a pipe
R	radius of curvature
R^+	variable defined by Rv_j^*/ν_f
$\overline{\overline{R}}_d$	mean radius of fluid particles
R_j	particle number source and sink rate

R_w	tube radius
Re	Reynolds number
$(Re)_d$	particle Reynolds number
r	radial coordinate
r_d^*	non-dimensional radius
S_B, S_C	surface available to collision
S_j	particle source and sink rates per unit mixture volume due to j -th particle interactions such as disintegration or coalescence
S_{ph}	particle source and sink rates per unit mixture volume due to phase change
s	entropy
s_a	surface entropy per area
$\widehat{s}_k, \widehat{s}_{ki}$	weighted mean entropy at bulk phase and at interfaces
s_m	mixture entropy
T	temperature
$T_i, \overline{\overline{T}}_i$	instant and mean interface temperature
$\overline{\overline{T}}_k, \overline{\overline{T}}_{ki}$	mean temperature at bulk phase and at interface
T'_k	stress tensor
t	time
t_C	time required for bubble coalescence
t_j	time when the j^{th} -interface passes the point
t_α^m (or t_α)	hybrid tensor of interface, see Aris (1962)
U	velocity of shock in mixture
U_0	velocity of stream
U_B, U_C	volume available to collision
u	internal energy
u_a	surface energy per area
u_b	mean fluctuation velocity
u_B, u_C	bubble velocity
u_e	eddy velocity
$\widehat{u}_k, \widehat{u}_{ki}$	weighted mean internal energy at bulk phase and at interfaces
u_m	mixture internal energy

u_{rW}	averaged relative velocity between leading bubble and bubble in wake region
u_t	root-mean-square approaching velocity of two bubbles
$u_{t,crit}$	critical fluctuation velocity
V	volume
\dot{V}	time derivative of volume V
V_c	critical bubble volume
V_{gi}^+	non-dimensional drift velocity
V_i	interfacial region
V_{kj}	drift velocity
V_{km}	diffusion velocity
V_m	fixed mass volume
V_s^*	ratio of $V_{s,min}$ to $V_{s,max}$
V_W	effective wake volume
V_{1p}	peak bubble volume in group 1
v	velocity
v'_f	liquid velocity fluctuation independent of bubble agitation
v''_f	liquid velocity fluctuation dependent on bubble agitation
v_f^*	friction velocity
v_g	average center-of-volume velocity of dispersed phase
v_i	velocity of interface
$\widehat{v}_k, \widehat{v}_{ki}$	weighted mean velocity at bulk phase and at interfaces
$\overline{(v'_k)^2} / 2$	mean turbulent kinetic energy
v_m	mixture center of mass velocity
v_{pm}	average local particle velocity weighted by particle number
v_r	relative velocity
$\overline{v_r}$	difference between area averaged mean velocities of phases
$v_{r\infty}$	relative velocity of a single particle in an infinite medium

v_s	velocity of interfacial particles
W_{ki}^T	work due to fluctuations in drag forces
We	Weber number
We_{crit}	critical Weber number
\mathbf{X}	convective coordinates
\mathbf{x}	spatial coordinates
x	spatial coordinate
y	spatial coordinate
y^+	variable defined by yv_f^*/ν_f
z	spatial coordinate

Greek

α_b	void fraction in slug bubble section
α_{core}	ratio of liquid-film cross-sectional area to total cross-sectional area
α_d	average overall void fraction
α_{drop}	ratio of cross-sectional area of drops to cross-sectional area of core
$\alpha_{g,crit}$	critical void fraction when center bubble cannot pass through free space among neighboring bubbles
$\alpha_{g,max}$	maximum void fraction
α_k	time (void) fraction of phase k
β	ratio of mixing length and width of wake
β_C	variable to take account of overlap of excluded volume
β_k	thermal expansivity based on averaged properties
Γ	constant
Γ_k	mass generation for phase k
γ	constant
γ_k	ratio of specific heats
Δ_a	interfacial entropy generation per area
Δ_k	entropy generation for phase k
$\Delta\dot{m}_{12}$	inter-group mass transfer rates from group 1 to group 2
Δt	time interval of averaging
Δt_B	time interval to drive daughter bubble apart with

	characteristic length of D_b
Δt_C	time interval for one collision
$\Delta t_k, \Delta t_s$	time intervals associated with phase k and interfaces
Δt_W	average time interval for a bubble in wake region to catch up with preceding bubble
δ	thickness of interface
δ	film thickness
δ'	collective parameter
δ_{crit}	critical film thickness where rapture occurs
δ_{init}	initial film thickness
δp_k	pressure deviation from saturation pressure
$\delta\mu$	volume element in μ space
ε	energy dissipation rate per unit mass
2ε (or $2\varepsilon_j$)	time associated with the j^{th} -interface
ε^{SI}	dissipation of shear-induced turbulence
$\varepsilon', \varepsilon''$	eddy diffusivity
η_{ph}	rate of volume generated by nucleation source per unit mixture volume
η_0	amplitude
Θ	contact angle
θ	angle in cylindrical coordinates
θ_w	wake angle
κ_{fr}	variable defined by $1 - \exp\left(-C_{fr} V_s^{+1/2} / D^{1/2}\right)$
κ_{Sk}, κ_{Tk}	isentropic and isothermal compressibilities of phase k
Λ_k	interfacial thermal energy transfer term in the averaged equation
λ	wavelength
λ	constant
λ_B	breakup efficiency
λ_C	coalescence efficiency
λ_c	critical wavelength
λ_k	bulk viscosity
μ	viscosity
$\overline{\mu}_k, \mu_k^T$	mean molecular and turbulent viscosities

μ_k^{T*}	mixing length coefficient
μ_m	mixture viscosity
ν	kinematic viscosity
ν_t	turbulent kinematic viscosity
ξ	particle (phase) velocity in Boltzmann statistical average
ξ	ratio of V_{1p} to V_c
ξ	variable defined by $2(1 - 0.2894D_{cl}^{*3})^2$
ξ	variable defined by P_i/P_{wf}
ρ	density
ρ_a	surface mass per area
$\overline{\rho_k}, \overline{\rho_k}$	partial and mean densities
ρ_k'	modified density defined by $\rho_k \coth(kh_k)$
ρ_m	mixture density
σ	surface tension
\mathcal{T}	viscous stress tensor
\mathcal{T}^D	diffusion (or drift) stress tensor
\mathcal{T}_f^{BI}	bubble-induced turbulent stress tensor
\mathcal{T}_f^{SI}	shear-induced turbulent stress tensor
$\overline{\mathcal{T}}, \mathcal{T}^T$	mixture viscous and turbulent stress tensors
$\overline{\mathcal{T}}_k, \mathcal{T}_k^T$	average viscous and turbulent stress tensor
\mathcal{T}_k^μ	average viscous stress
$\overline{\mathcal{T}}_{ki}, \mathcal{T}_{ki}$	interfacial shear stress
τ_C	contact time for two bubbles
τ_i	interfacial shear stress
τ_o	reference time constant
τ_{tk}, τ_{nk}	tangential and normal stresses at interface
τ_{wf}	wall shear
Φ	velocity potential
Φ_k^T	turbulent work effect in enthalpy energy equation
Φ_m^i	interfacial mechanical energy exchange effect in the mixture thermal energy equation
Φ_k^μ	viscous dissipation

Φ_m^μ	mixture viscous dissipation
Φ_m^σ	surface tension effect in the mixture thermal energy equation
ϕ	source term
ϕ_a	interfacial source per area
ϕ_j	source and sink rate for interfacial area concentration
ϕ_k	velocity potential
χ	coefficient accounting for contribution from inter-group transfer
ψ	property of extensive characteristics
ψ	shape factor
$\widehat{\psi}, \widehat{\psi}_k$	mass weighted mean values for mixture and phase k
ψ_a	property per interfacial area
Ω	potential function

Subscripts and Superscripts

a	surface (property per area)			
c	continuous phase			
d	dispersed phase			
f	liquid phase			
g	vapor phase			
i	interface			
j	j^{th} -interface			
k	each phase : ($k=1$ & 2), ($k=c$ & d), ($k=f$ & g)			
ki	k^{th} -phase at interfaces			
m	<table> <tr> <td rowspan="2" style="font-size: 2em; vertical-align: middle;">{</td> <td>mixture (in macroscopic formulation)</td> </tr> <tr> <td>fixed mass (in local instant formulation)</td> </tr> </table>	{	mixture (in macroscopic formulation)	fixed mass (in local instant formulation)
{	mixture (in macroscopic formulation)			
	fixed mass (in local instant formulation)			
n	normal to interface			
o	reference			
RC	random collision			
r, θ, z	cylindrical coordinate			
sat	saturation			
s	<table> <tr> <td rowspan="2" style="font-size: 2em; vertical-align: middle;">{</td> <td>surface (surface property per mass)</td> </tr> <tr> <td>solid phase</td> </tr> </table>	{	surface (surface property per mass)	solid phase
{	surface (surface property per mass)			
	solid phase			

SI	surface instability
SO	shearing off
TI	turbulent impact
WE	wake entrainment
t	tangential to interface
w	wall
x, y, z	rectangular coordinate
$+, -$	+ and - side of shock in macroscopic field
$1, 2$	phase 1 and phase 2

Symbols and Operators

A	tensor
\mathbf{A}	vector
A	scalar
$\mathbf{A} \cdot \mathbf{B}$	dot product
\mathbf{AB}	dyadic product of two vectors (=tensor)
$\mathbf{A}:\mathbf{B}$	double dot product of two tensors (=scalar)
$\nabla \cdot$	divergence operator
∇	gradient operator
$\nabla_s \cdot$	surface divergence operator (Aris, 1962)
$(\mathbf{A})^+$	transposed tensor
$\frac{D_k}{Dt}$	$= \frac{\partial}{\partial t} + \widehat{\mathbf{v}}_k \cdot \nabla$
$\frac{D}{Dt}$	$= \frac{\partial}{\partial t} + \mathbf{v}_m \cdot \nabla$
$\frac{D_c}{Dt}$	$= \frac{\partial}{\partial t} + \mathbf{C}_k \cdot \nabla$
$\frac{D_i}{Dt}$	$= \frac{\partial}{\partial t} + \widehat{\mathbf{v}}_i \cdot \nabla$
$\frac{d_s}{dt}$	surface convective derivative with $\widehat{\mathbf{v}}_s$ (Aris, 1962)
\overline{F}	time average
\overline{F}^w	weighted mean value
\overline{F}^{w_k}	k^{th} -phase weighted mean value
$\overline{\overline{F}}$	phase average

$\widehat{\psi}_k$	k^{th} -phase mass weighted mean value
$\widehat{\psi}$	mixture mass weighted mean value
F'_k	fluctuating component with respect to mean value
F'_{ki}	fluctuation component with respect to surface mean value
$\overline{F_{(i)}}, \overline{F_{ki}}$	surface average
\widehat{F}_{ki}	mass flux weighted mean value at interfaces
$(\)_{,\beta}$	surface covariant derivative (Aris, 1962)
$[\Delta t]_k$	with $(k=T,S,1,2)$; sets of time intervals
\sum_k	summation on both phases
\sum_j	summation on the interfaces passing in Δt at \boldsymbol{x}

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